



Ditch Upgrade Results in Energy Savings at North Cary WRF

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WATER TECHNOLOGIES

AGENDA

- Intro to Veolia's Ditch Technologies
- Key Benefits for WWTPs
- Upgrade Reference
- Advanced Online Control
- Questions??



VEOLIA WATER TECHNOLOGIES INSTALLATIONS

Approximately 100 Veolia Ditch Installations in the United States

- ~ 20% < 1 MGD
- ~ 60% 1 - 5 MGD
- ~ 20% > 5 MGD

Over 50% of these are BIO-DENITRO™ systems

30+ years applying this technology

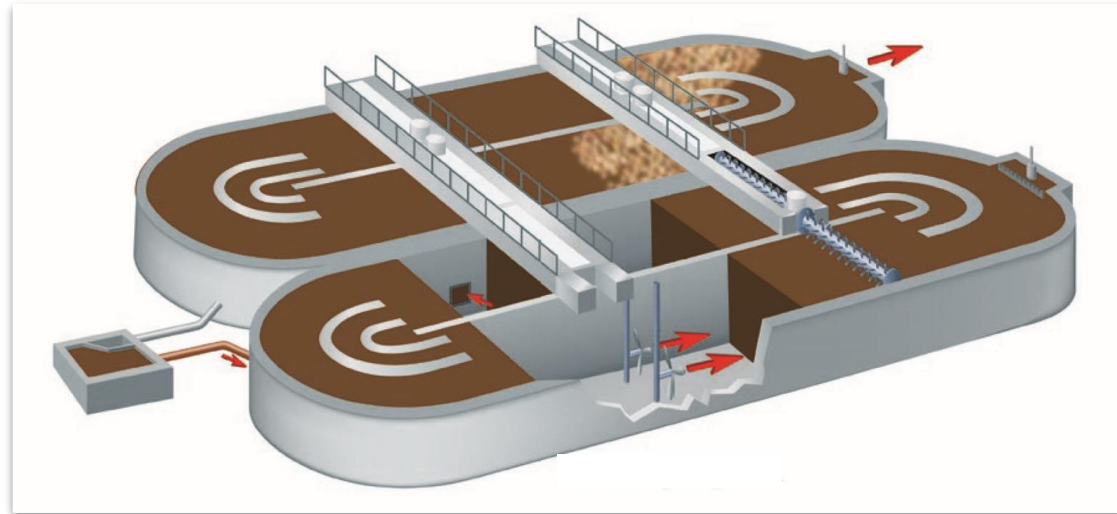
Phased control for superior effluent quality



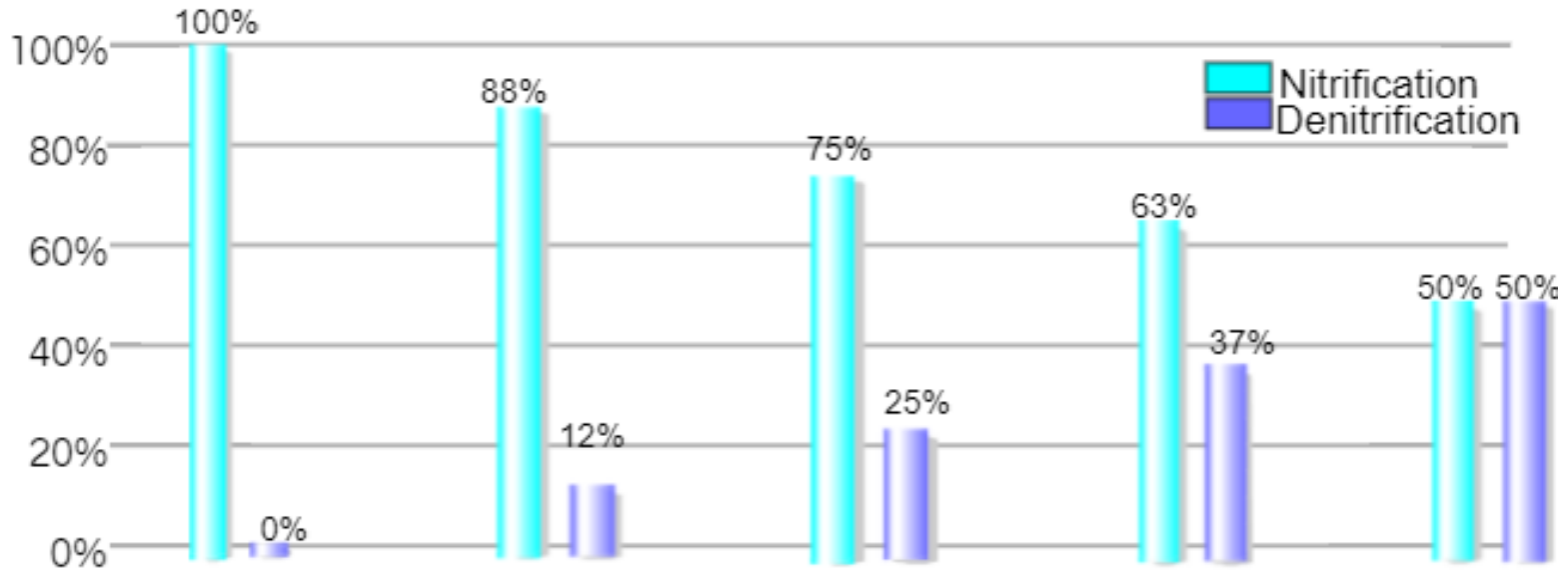
BIO-DENITRO™

BENEFITS

- Highly controlled N and P removal
- No internal mixed liquor recycle pumping
- Separation of mixing and aeration
- * Unlimited aeration turndown
- Operational flexibility
- TN < 4-5 without secondary anoxic zones



PHASING WITH TIME BASED CONTROL



Resulting Volume Allocation (%)



CASE STUDY

NORTH CARY, NC BIO-DENIPHO™

References



CASE STUDY GOALS

NORTH CARY, NC BIO-DENIPHO™

Primary Goal of Project:

Upgrading the Plant's aeration capacity from 12 MGD to 15 MGD without adding additional process volume meeting the existing effluent limits of the Plant

- TN < 3 mg/L
- TP < 1.0 mg/L
- NH₄-N < 0.5 mg/L

Secondary Goal of Project:

Operate the Plant without addition of external carbon nor chemical precipitation of phosphorus



CASE STUDY PROJECT

NORTH CARY, NC BIO-DENIPHO™

- Replace existing rotors with diffused air for increase aeration capacity
- Installation of new blower station (centrifugal blowers)
- Existing Wilo mixers remain in place for mixing during anoxic phase
- Installation of online ammonium and nitrate analyzers
- Upgrading the control of the Plant from time-based control to real-time PLC online control



CASE STUDY RESULTS

NORTH CARY, NC BIO-DENIPHO™

- Operating two out of three trains. Current hydraulic load 7.0 MGD
- Reduction of about 6% of energy overall at the Plant
 - Centrifugal blowers with blow-off valves utilized
- Average effluent values before and after the upgrade of the Plant
- Deeper understanding of the biological process through online measurements of nutrients

Effluent Values	Before (Jan - Dec 2022)	After (Oct-2022- Sep 2023)
TN (mg/L)	1.95	1.79
TP (mg/L)	0.34	0.27



HUBGRADE PERFORMANCE

History, Overview and Main Usage



HUBGRADE PERFORMANCE DIGITAL TWIN TO OPTIMIZE MUNICIPAL & INDUSTRIAL PLANTS WORLDWIDE

15
Patents



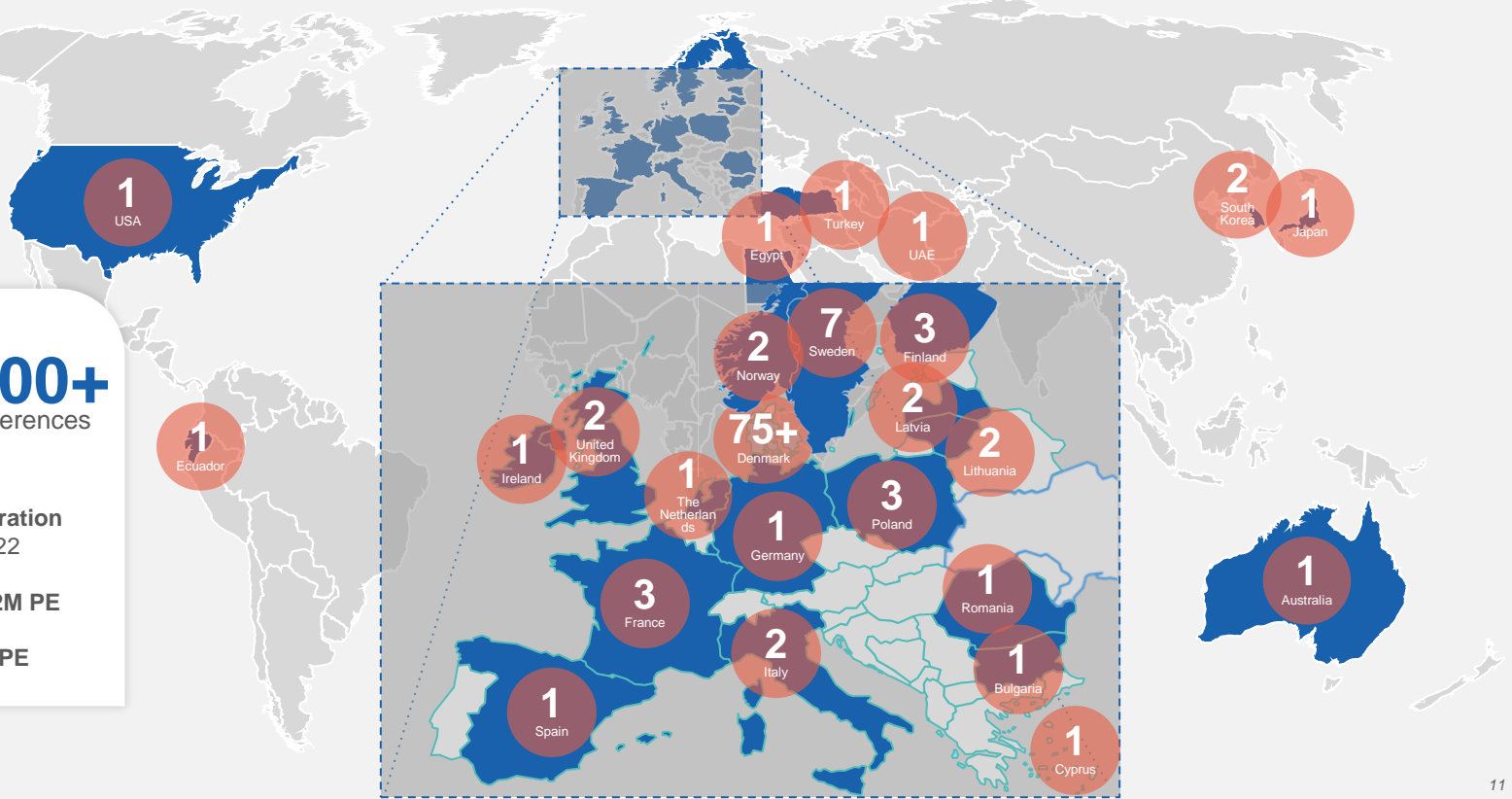
30+
years of experience

100+
references

1000+ years of operation
from 1992 to 2022

WWTP from 2k to 2M PE

More than 20 M PE



ADVANCED OPTIMIZATION

WHY ?



Reduced operating costs

- Reduced energy consumption
- Increased energy production
- Reduced chemical consumption



Increased hydraulic capacity

- Reduced overflow / bypass
- Increased flow through existing plant
- Less / avoided CAPEX



Increased biological capacity

- Increased biological load
- Improved effluent quality
- Less / avoided CAPEX



Increased capacity of sewer

- Reduced combined sewer overflow (CSO)
- Save extension of retention basin volume
- Less / avoided CAPEX



Compliance and stable operation

- Stability results in savings
- Meet your targets
- Easy for operator to perform
- Continuously acting to the actual situation in load and flow



HUBGRADE PERFORMANCE PLANT

TYPICAL OPEX SAVINGS RANGES



Less energy consumption

- Aeration | 10 – 30 %
- Mixing | 25 – 75 %
- Internal pumping | 25 – 75 %



Less chemical dosage

- P-precipitation | 20 – 100 %
- Dosage of COD, N & P | 25 – 100 %



Less chemical sludge production

- Equivalent to less P-precipitation dosage



Higher Hydraulic / Biological capacity

- 20 – 100 % higher flow
- 10 – 40 % more load



Better effluent quality

- Total-N | 20 – 50 %
- Total-P, BOD, COD, SS... | 0 – 50 %



Better footprint – more valorised products

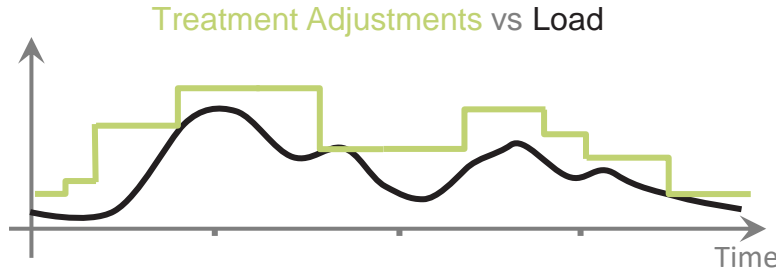
- CO_{2-eq} reduction 10 – 30%
- Gaz production up to +5%
- P harvesting increased up to total P removal
- N₂O reduction 50 - 90%



REAL TIME OPTIMIZATION

FASTER, BROADER AND CHEAPER

Traditional Operation



Optimization

+



WWTP Experts

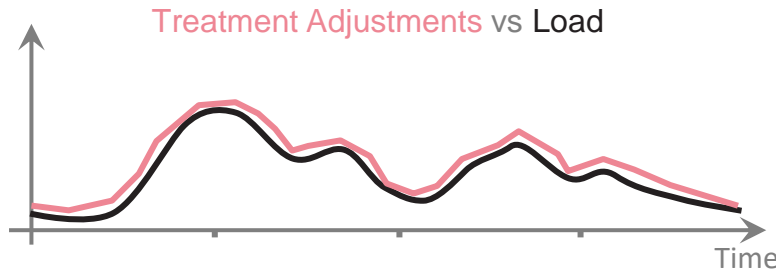


PLC / SCADA



Smart Sensors / Equipments

With Digital Twin

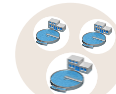


Optimization

+++



WWTP & Twin Experts



RT Multiple optimisation loops



RT Comparison with similar optimized plants



Predictive Model with weather & Grid Forecast

DO & N REMOVAL

COMPLIANT COD REMOVAL WITH LESS ENERGY



DO & Nitrogen Removal

AI

WHY ?

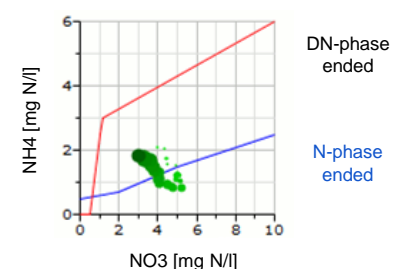
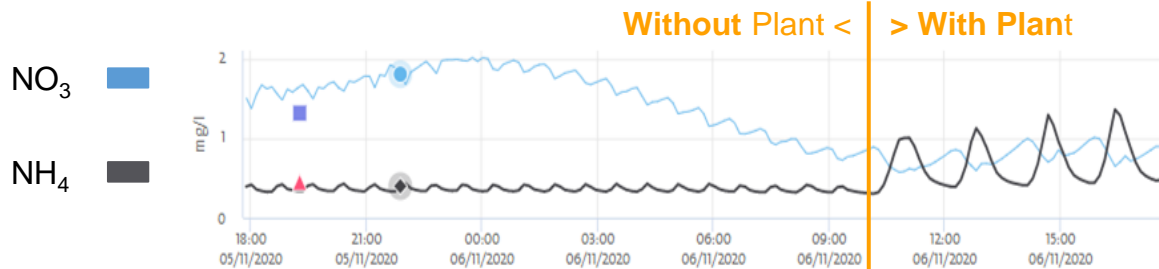
- Ensure compliance
- Reduce OPEX
- Reduce energy use
- Reduce CO₂ emissions

HOW ?

- Avoid over-aeration & enhance the usage of COD for NO₃ removal.
- Enhance balancing of N/DN processes according to load variations.

WHAT ?

- Two patented optimized controls:
- regulating the DO set point
 - regulating N/DN switching phases.
- Providing set points for intermittent aeration and oxygen based on real-time measurements of NO₃ and NH₄ in the aeration tanks.

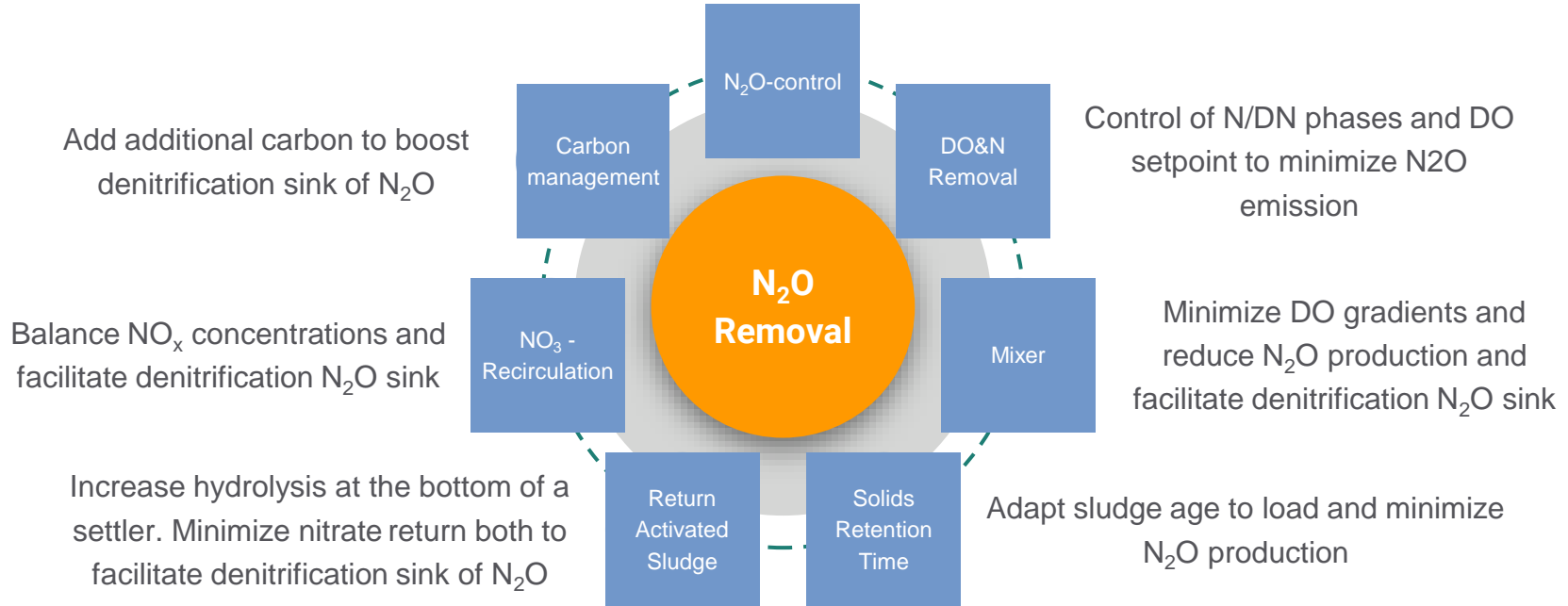


N₂O REMOVAL

ADVANCED OPTIMISATION IN ACTION



Abort aeration and enforce denitrification sink of N₂O according to N₂O threshold measurements online



SMART BIO-P[®] IN DETAILS

GROW BACTERIA DURING LOW LOAD



OPEX



Chemicals



Compliance



Capacity



Smart Bio-P

WHY ?

- Enhance biological P-removal
- Reduction of chemicals OPEX



HOW ?

- Real time control of aeration phases to create temporary anaerobic phases during low load (NH₄+NO₃) & low flow



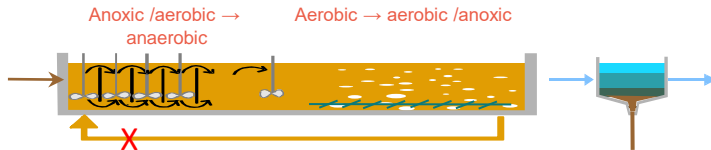
WHAT ?

- Find a time slot for growth of Bio-P bacteria somewhere in existing volume.

Adaptable to all activated sludge plant designs

Pre DN - Plugflow - MLE

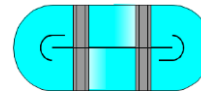
Change of process in the upstream anoxic/aerobic sections to temporary anaerobic



One tank/single ditch - Azenit™

Change of process to temporary anaerobic

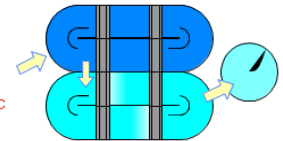
Aerobic/Anoxic → Aerobic/Anoxic/Anaerobic



BioDenitro™/BioDenitro™

Change of process in inlet section to temporary anaerobic

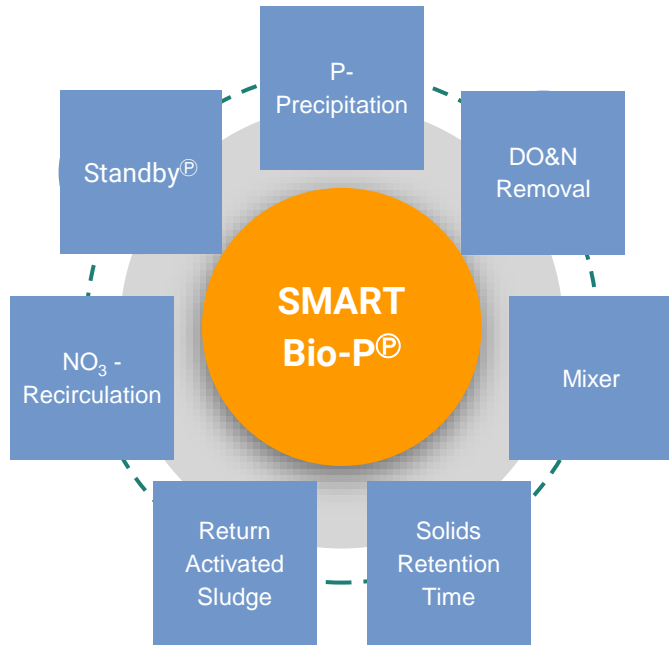
Anoxic → Anaerobic
Aerobic/anoxic





SMART BIO-P[®]

P-REMOVAL DOSAGE & BIOLOGICAL P-PRECIPIATION



Why use SMART Bio-P?

Aim: Do it better and cheaper

Key idea:

Find a time slot for growth of Bio-P bacteria somewhere in existing volume

Save CAPEX

For construction/reconstruction of anaerobic volume

Save OPEX

Dosage for co-P-precipitation and/or

Dosage for post P-precipitation Handling of chemical sludge

REFERENCES - Reduction in chemical for precipitation

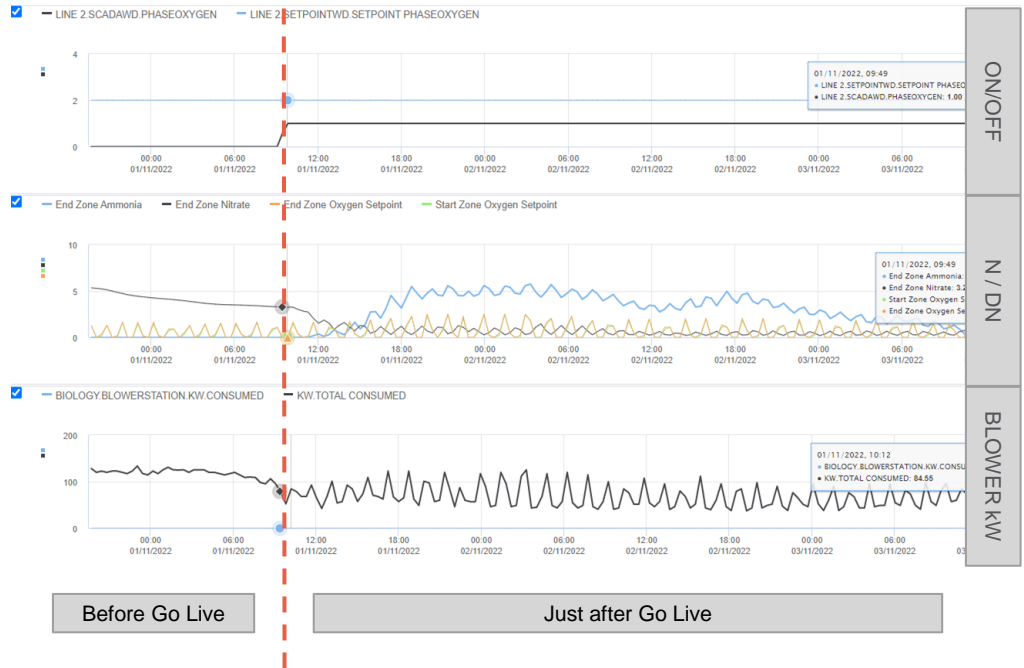
- **Helsingør WWTP, DK (75.000PE)**
→ 80% Reduction
- **Nosedo WWTP, IT (1.250.000PE)**
→ 70% Reduction
- **EDE, NL (300.000PE)**
→ 20% Reduction
- **Riga, LV (750.000 → 1.050.000 PE)**
→ Extension without Bio-P Tank



47000 PE - OMAGH WWTP, NORTHERN IRELAND

SMOOTH, FAST AND PROVEN PROCESS - 5 MONTHS

CONFIDENTIAL



ENERGY COSTS

35K€ saved

SPECIFIC ENERGY CONSUMPTION

Reduced by 45%

KWH DAILY AVERAGE CONSUMPTION

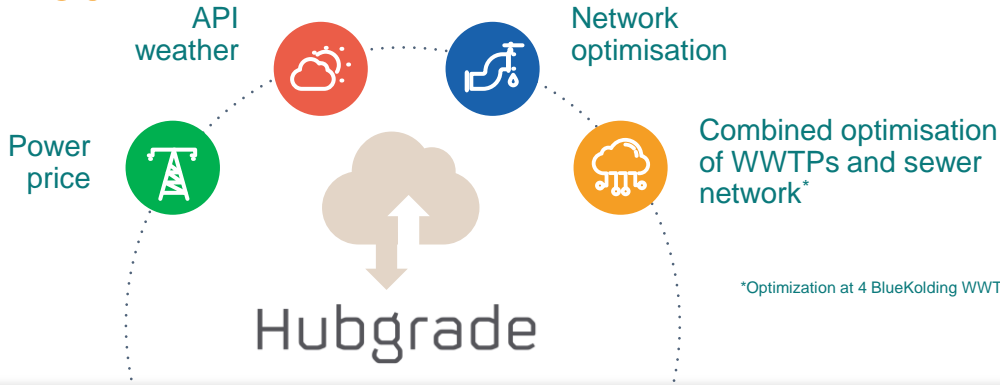
Reduced by 32%





CASE STUDY - HPP

BLUEKOLDING - 90k PE



*Optimization at 4 BlueKolding WWTPs, in connection with Sewer



Drivers

- Reduces **operating costs**
- + Increased **hydraulic & biological capacity**

Benefits

- Increased **capacity of sewer**
- **Compliance** and stable operation
- **Improved operation**, staff advantages, data handling and reporting

Reduced:

Nitrogen	- 27%
Chemical	- 46%
Energy consumption	- 23%
Overflow	- 83%

Increase:

Hydraulic capacity	+ 80%
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Thank You!
Questions?



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